

PRINCIPLES OF MATHEMATICAL MODELLING

3. MODEL OF BIOREACTOR

3.1. Growth model with nutrition restriction

In the case of no restriction on nutritions, growth is described by

$$P' = bP$$

When nutrition is restricted (there is no renewal of nutrition)

- increase of population, decrease of nutrition amount (decrease of availability)
- decrease of growth rate

Anotate

- $S(t)$ - nutrition concentration
- $P(t)$ - population concentration

Remark.

- volume $\cdot S(t)$ - total amount of nutrition
- $N(t) = \text{volume} \cdot P(t)$ - total population size

Growth rate (b) depends on $S \rightarrow b(S)$

Assumptions on $b(S)$

- $S = 0$ - no nutrition \rightarrow no growth
 $\rightarrow b(0) = 0$
- Nutrition amount is unrestricted - $S = \infty \rightarrow$ exponential growth
 $\rightarrow b(\infty) = V$

Simplest function b satisfying

$$b(0) = 0 \quad \text{i} \quad b(\infty) = V$$

is

$$b(S) = V \frac{S}{K + S}$$

Jacques Monod

- 1910, Paris, France – 1976., Cannes, France
- 1965. Nobel Prize in Physiology or Medicine
- One of founders of molecular biology
- J. Monod (1949). The growth of bacterial cultures, *Ann. Rev. Microbiol.*, 3, 371—393
- Studied growth rate for bacterial cultures of Escherichia Coli K12.
- Dependence of growth rate on nutrition concentration (glucose)
- Growth rate is constant when concentration of glucose (S) is constant: $P' = b(S) P$.
- Experimentally determined **specific growth rate** for fixed glucose concentrations

Experimentally determined relation between specific growth rate and nutrition concentration:

$$b(S) = V \frac{S}{K + S}$$

- Monod function
- V - maximal specific growth rate
- K - half-saturation constant = nutrition concentration when specific growth rate equals to half of maximal specific growth rate

Now, population growth rate is given by

$$P'(t) = V \frac{S(t)}{K + S(t)} P(t)$$

Mass conservation: total mass of a system is constant

→ Whole nutrition transforms into biomass.

- Population mass = volume $\cdot P(t) \cdot m_P$
(m_P mass of one cell)
- Nutrition mass = volume $\cdot S(t) \cdot m_S$
(m_S unit mass for nutrition)

$$\text{volume} \cdot P(t) \cdot m_P + \text{volume} \cdot S(t) \cdot m_S = \text{const}$$

Define $Y = \frac{m_S}{m_P}$

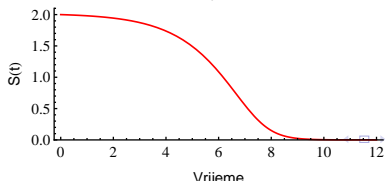
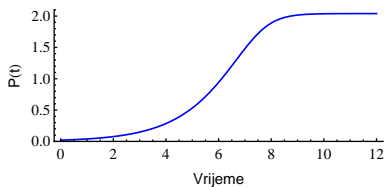
$$Y S(t) + P(t) = \text{const} \quad \Leftrightarrow \quad \frac{d}{dt}[Y S(t) + P(t)] = 0$$

$$\Rightarrow S'(t) = -\frac{P'(t)}{Y} = -V \frac{S(t)}{K + S(t)} \frac{P(t)}{Y}$$

Monod model

$$P'(t) = V \frac{S(t)}{K + S(t)} P(t)$$

$$S'(t) = -V \frac{S(t)}{K + S(t)} \frac{P(t)}{Y}$$



From

$$Y S + P = C$$

it follows

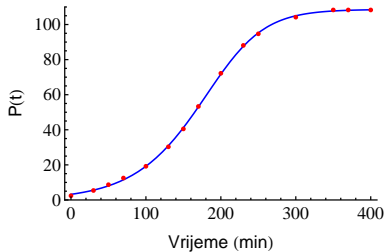
$$S = \frac{1}{Y}(C - P)$$

$$\begin{aligned} P' &= V \frac{S}{K + S} P \\ &= \frac{V}{Y} \frac{C - P}{K + \frac{1}{Y}(C - P)} P \\ &= \frac{V(C - P)}{K Y + C - P} P \end{aligned}$$

$$P' = \frac{V(C - P)}{K Y + C - P} P$$

Model describes experimental data well.

Data for E. coli growth



Phase portrait of the system.

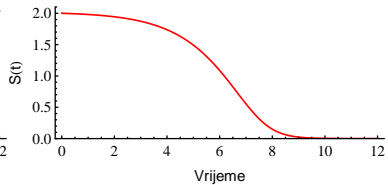
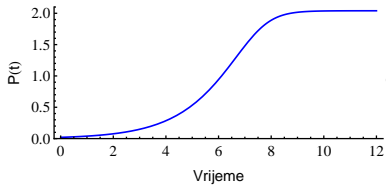
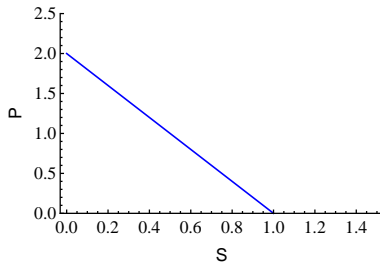
- Parametric graph $\{(S(t), P(t)) | t \geq 0\}$

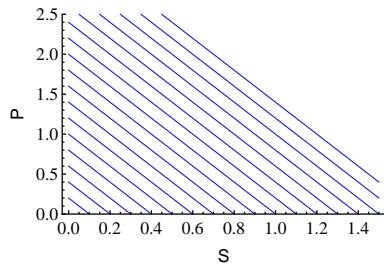
Monod model:

$$P + Y S = C$$

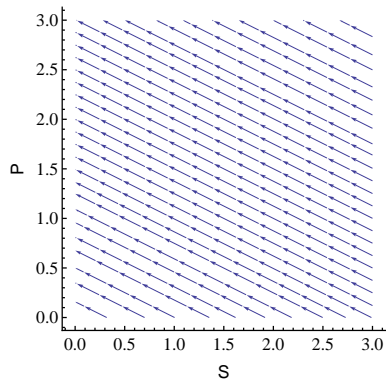
Linear relation.

C is defined by initial conditions: $C = P(0) + Y S(0) = P_0 + Y S_0$





Phase portrait for Monod model



3.2. Growth and quiescence

When nutrition is consumed, cells may go to the **quiescence** stage.
Here they can be for a long time.

Introduce another cell population (quiescent cells), Q :

- S - concentration (limited) of nutrition
- P - proliferating cells population (concentration)
- Q - quiescent cells population (concentration)

We start from the previous model:

$$S' = -V \frac{S}{K+S} \frac{P}{Y}$$

$$P' = V \frac{S}{K+S} P - Q'$$

$$Q' = ?$$

Remark.

Quiescent cells do not consume nutrition. \rightarrow S' does not depend on Q

Assumptions:

- Transfer rate from $P \rightarrow Q$ is proportional to P
- Transfer rate from $Q \rightarrow P$ is proportional to Q
- Both depend on S (nutrition concentration):

$$Q' = \alpha(S)P - \beta(S)Q$$

Choice of functions $\alpha(S)$ and $\beta(S)$:

- Sufficient concentration of nutrition (S large)
 $\rightarrow \alpha(S) \approx 0$ i $\beta(S) > 0$
- No nutrition ($S \approx 0$)
 $\rightarrow \alpha(S) > 0$ i $\beta(S) \approx 0$
- $\alpha(0) > 0$, $\alpha(\infty) = 0$ i
 $\beta(0) = 0$, $\beta(\infty) > 0 \rightarrow$

$$\alpha(S) = \frac{1}{1+S} \quad \text{i} \quad \beta(S) = \frac{S}{1+S}$$

Model:

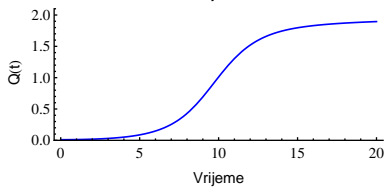
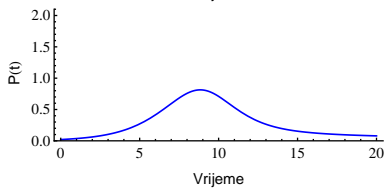
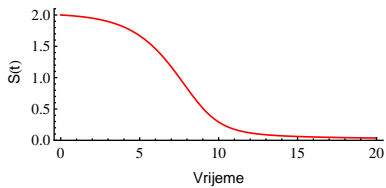
$$S' = -V \frac{S}{K+S} \frac{P}{Y}$$

$$P' = V \frac{S}{K+S} P - \alpha(S)P + \beta(S)Q$$

$$Q' = \alpha(S)P - \beta(S)Q$$

Remark. If we model death instead of quiescence.

There is no transfer $Q \rightarrow P$, $\beta \equiv 0$

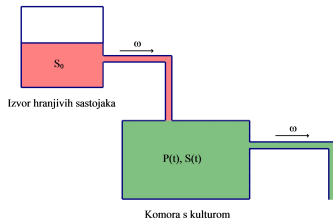


3.3. Chemostat model

Monod model - growth in closed system.

No nutrition inflow or removal of the part of population.

It is possible to grow cell culture in fixed volume where nutrition is constantly regenerated by the flow of media.



- In the chamber (in media) are cells and nutrition (substrat)
- They are ideally mixed (cell concentration and nutrition concentration in chamber are uniform)
- Substrat by constant flow inflows into the chamber
- Content of the chamber outflows by the same speed (keeping a volume constant).
- ω - washout rate = flow speed (volume/time) / chamber volume

- Such bioreactor is named **chemostat** (**Chemical environment is static**)
- or **CSTR** (*continuously stirred tank reactor*)
- Inflow of nutrition/substrat may be regulated
- Temperature, oxygen concetration may be also regulated, . . .
- Several populations may be grown in the same time (in different interactions)
- biological model for complex ecosystems

Derivation of the model

Change of substrat concentration:

Q' = inflow from the tank - consumption by population - wash out

Change of population concentration:

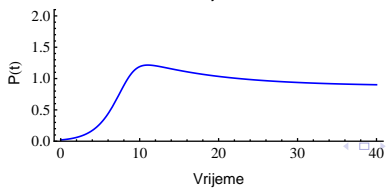
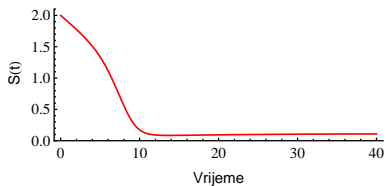
P' = division - wash out

- speed of division: $V \frac{S}{K + S} P$ (Monoda function)
- speed of substrat consumption: $V \frac{S}{K + S} \frac{P}{Y}$
- speed of substrat inflow: ωS_0
 - Total inflow (speed): $\omega \nu$ (ν - volumen komore)
 - Total substrat inflow: $\omega \nu S_0$
 - Increase of substrat concentration: $\omega \nu S_0 / \nu = \omega S_0$
- Total outflow (speed):: $\omega \nu$ (= ukupan dotok)
 - Outflow - population: $\omega P(t)$
 - Outflow - substrat: $\omega S(t)$

Chemostat model.

$$S' = -V \frac{S}{K+S} \frac{P}{Y} + \omega S_0 - \omega S$$

$$P' = V \frac{S}{K+S} P - \omega P$$



Biofilm.

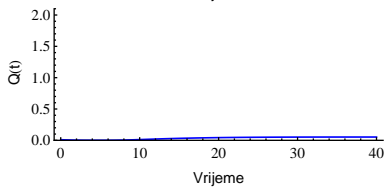
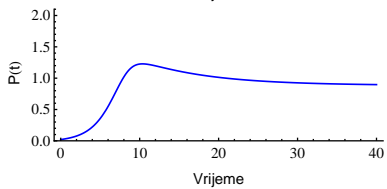
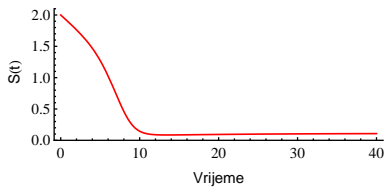
- Tijekom rasta u komori stanice se mogu početi lijepiti za stijenku komore.
- → Biofilm.
- Sada se u komori nalaze
 - stanice koje slobodno plutaju u mediju (P)
 - stanice priljepljene za zid komore (Q)
- Stanice priljepljene za zid komore
 - imaju drugačiju potrošnju hranjivih sastojaka (manja dostupnost)
 - manja specifična brzina rasta
 - ne istječu s medijem iz komore
- Stanice se priljepljuju za stijenku komore brzinom $\alpha = \alpha(S)$ (prijelaz iz populacije P u populaciju Q)
- Uslijed protoka medija, stanice se odljepljuju od stijenke komore brzinom $\beta = \beta(S)$ (prijelaz iz populacije Q u populaciju P)

Model:

$$S' = -\frac{VS}{K+S} \frac{P}{Y} - \frac{V_Q S}{K_Q+S} \frac{P}{Y} - \omega(S - S_0) S$$

$$P' = V \frac{S}{K+S} P - \omega P - \alpha(S) P + \beta(S) Q$$

$$Q' = \frac{V_Q S}{K_Q+S} P + \alpha(S) P - \beta(S) Q$$



Hranidbeni lanac.

Rast s ograničenim hranjivim sastojcima

- U posudi su tri vrste mikroba (P_1, P_2, P_3).
- Populacija P_1 konzumira supstrat S_1 koji se nalazi u posudi.
- P_1 proizvodi supstrat S_2 za populaciju P_2
- P_2 proizvodi supstrat S_3 za populaciju P_3
- $S_1 \rightarrow P_1 \rightarrow S_2 \rightarrow P_2 \rightarrow S_3 \rightarrow P_3$
- Populacija P_1 supstrat S_2 proizvodi brzinom m_2
- Populacija P_2 supstrat S_3 proizvodi brzinom m_3

Krenut ćemo od Monodovog nodela.

Pretpostavljamo da sve stanice proizvode suptrat.

Izvedimo jednadžbu za populaciju P_1 . Rast populacije je opisan s:

$$P_1' = \frac{V_1 S_1}{K_1 + S_1} P_1$$

Proizvodnja supstrata: $m_2 P_1$.

Promjena supstrata S_1 :

$$S_1' = -\frac{V_1 S_1}{K_1 + S_1} \frac{P_1}{Y_1} - \frac{m_2}{Y_1} P_1$$

Jednadžbe:

$$P_1' = \frac{V_1 S_1}{K_1 + S_1} P_1$$

$$S_1' = -\frac{V_1 S_1}{K_1 + S_1} \frac{P_1}{Y_1} - \frac{m_2}{Y_1} P_1$$

Druga populacija analogno.

Povećanje koncentracije supstrata: $m_2 P_1$.

$$P_2' = \frac{V_2 S_2}{K_2 + S_2} P_2$$

$$S_2' = m_2 P_1 - \frac{V_2 S_2}{K_2 + S_2} \frac{P_2}{Y_2} - \frac{m_3}{Y_2} P_2$$

Isto i za populaciju P_3 , jedino što nema proizvodnje supstrata:

$$P_3' = \frac{V_3 S_3}{K_3 + S_3} P_3$$

$$S_3' = m_3 P_2 - \frac{V_3 S_3}{K_3 + S_3} \frac{P_3}{Y_3}$$

Model:

$$S_1' = -\frac{V_1 S_1}{K_1 + S_1} \frac{P_1}{Y_1} - \frac{m_2}{Y_1} P_1$$

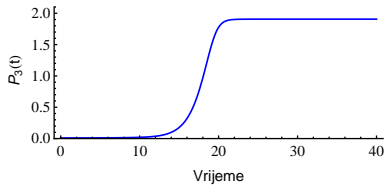
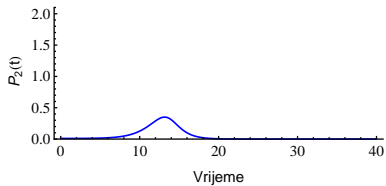
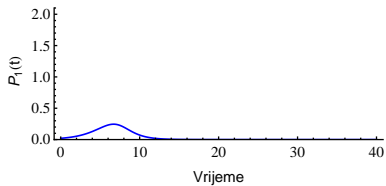
$$P_1' = \frac{V_1 S_1}{K_1 + S_1} P_1$$

$$S_2' = m_2 P_1 - \frac{V_2 S_2}{K_2 + S_2} \frac{P_2}{Y_2} - \frac{m_3}{Y_2} P_2$$

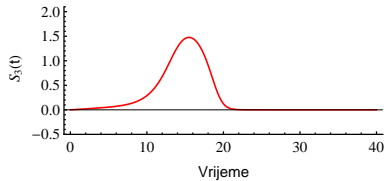
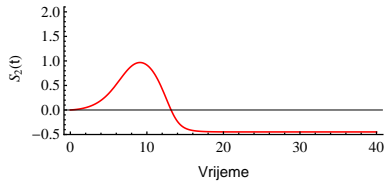
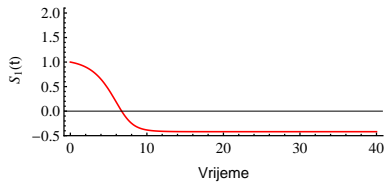
$$P_2' = \frac{V_2 S_2}{K_2 + S_2} P_2$$

$$S_3' = m_3 P_2 - \frac{V_3 S_3}{K_3 + S_3} \frac{P_3}{Y_3}$$

$$P_3' = \frac{V_3 S_3}{K_3 + S_3} P_3$$



Populacija se smanjuje!



Negativne koncentracije supstrata!

Stanice proizvode supstrat i kada više nemaju svojih hranjivih sastojaka!

Treba koristiti model s uključenim stanicama u mirovanju.

Supstrat proizvode samo aktivne stanice. Kada nema hranjivih sastojaka, stanice su u stanju mirovanja i nema proizvodnje supstrata.

Problem

Modificirajte prethodni model tako da uključite i populaciju stanica u mirovanju.

Rješenje.

$$S_1' = -\frac{V_1 S_1}{K_1 + S_1} \frac{P_1}{Y_1} - \frac{m_2}{Y_1} P_1$$

$$P_1' = \frac{V_1 S_1}{K_1 + S_1} P_1 - \alpha_1(S_1) P_1 + \beta_1(S_1) Q_1$$

$$Q_1' = \alpha_1(S_1) P_1 - \beta_1(S_1) Q_1$$

$$S_2' = m_2 P_1 - \frac{V_2 S_2}{K_2 + S_2} \frac{P_2}{Y_2} - \frac{m_3}{Y_2} P_2$$

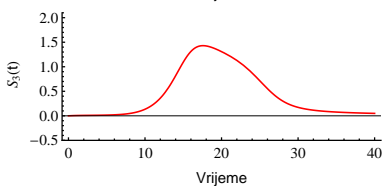
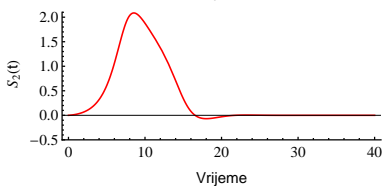
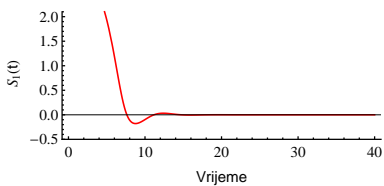
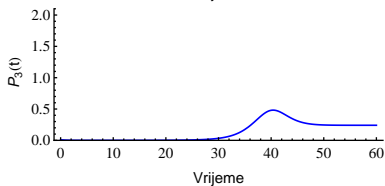
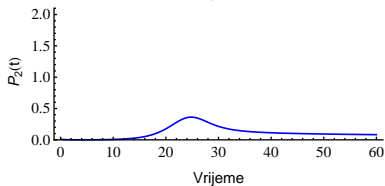
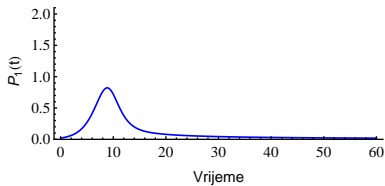
$$P_2' = \frac{V_2 S_2}{K_2 + S_2} P_2 - \alpha_2(S_2) P_2 + \beta_2(S_2) Q_2$$

$$Q_2' = \alpha_2(S_2) P_2 - \beta_2(S_2) Q_2$$

$$S_3' = m_3 P_2 - \frac{V_3 S_3}{K_3 + S_3} \frac{P_3}{Y_3}$$

$$P_3' = \frac{V_3 S_3}{K_3 + S_3} P_3 - \alpha_3(S_3) P_3 + \beta_3(S_3) Q_3$$

$$Q_3' = \alpha_3(S_3) P_3 - \beta_3(S_3) Q_3$$



Negativne koncentracije supstrata!

I dalje se troši supstrat kada ga nema.

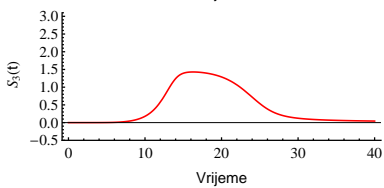
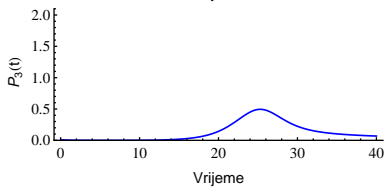
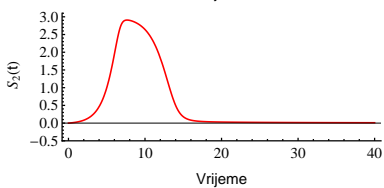
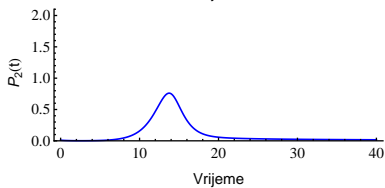
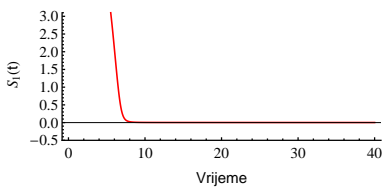
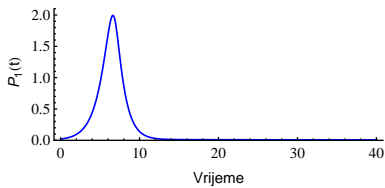
Modificirajmo proizvodnju supstrata.

Ako nema supstrata S_1 onda nema niti proizvodnje supstrata S_2 .

Proizvodnja:

$$\frac{S_1}{1 + S_1} m_2 P_1$$

$$\frac{S_2}{1 + S_2} m_3 P_2$$



Ako na isti način modificiramo model rasta s ograničenjem (bez populacije stanica u mirovanju) dobijamo

Model:

$$S_1' = -\frac{V_1 S_1}{K_1 + S_1} \frac{P_1}{Y_1} - \frac{S_1}{1 + S_1} \frac{m_2}{Y_1} P_1$$

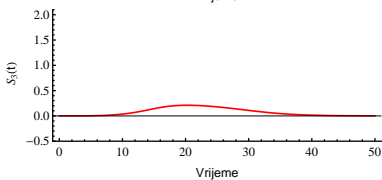
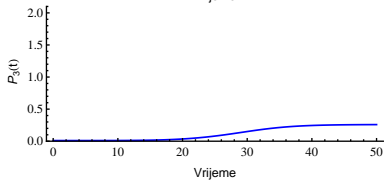
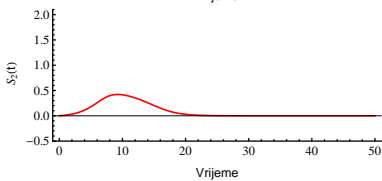
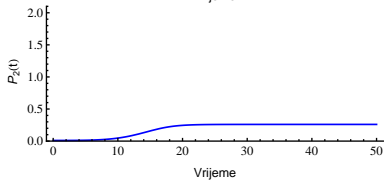
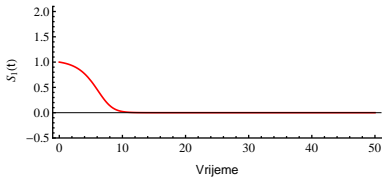
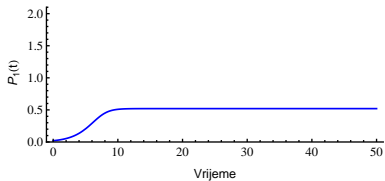
$$P_1' = \frac{V_1 S_1}{K_1 + S_1} P_1$$

$$S_2' = \frac{S_1}{1 + S_1} m_2 P_1 - \frac{V_2 S_2}{K_2 + S_2} \frac{P_2}{Y_2} - \frac{S_2}{1 + S_2} \frac{m_3}{Y_2} P_2$$

$$P_2' = \frac{V_2 S_2}{K_2 + S_2} P_2$$

$$S_3' = \frac{S_2}{1 + S_2} m_3 P_2 - \frac{V_3 S_3}{K_3 + S_3} \frac{P_3}{Y_3}$$

$$P_3' = \frac{V_3 S_3}{K_3 + S_3} P_3$$

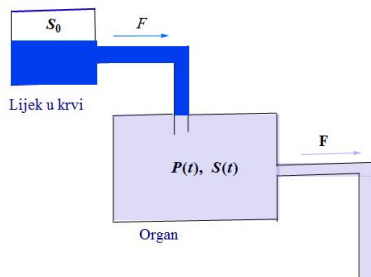


7. Domaća zadaća

Izvedite model hranidbenog lanca s tri populacije za rast u chemostatu.

4.4. Model infuzije lijeka

Modifikacija 'chemostat' modela se može iskoristiti kao jednostavan model utjecaja lijeka u krvi (npr. kemoterapija).



Ovdje je S_0 - koncentracija lijeka u krvi koja ulazi u organ (u 'chemostat' modelu je to bila oznaka za koncentraciju hranjivih sastojaka).

- $P(t)$ - broj stanica izloženih lijeku (pretpostavka: sve su stanice jednake mase)
- V volumen krvi u organu, tj. volumen krvi u području u kojem se stanice tretiraju.
- $F = F_{in} = F_{out}$ - brzina protoka krvi (l/s)
- $S_0, S(t)$ - koncentracija lijeka

Pretpostavka: stanice i lijek u organu su 'dobro izmiješani'.
Realističniji modeli npr. uključuju da lijek djeluje samo na vanjske stanice tumora.

F je brzina toka krvi koja arterijom dolazi u organ i izlazi iz njega..

Glavna razlika u odnosu na 'chemostat' model:

- stanice se razmnožavaju brzinom koja je, u principu, nezavisna o lijeku.
- ali lijek ima negativni utjecaj na rast populacije stanica ubijajući ih.
Brzinu ubijanja opisujemo nekom funkcijom $K(S)$.
- krv na izlazu sadrži samo (neiskorišteni) lijek a ne i stanice.

Pretpostavke su:

- stanice se razmnožavaju eksponencijalno
- brzina ubijanja je proporcionalna s $K(S) \cdot P$.

Uočimo da je brzina ubijanja stanica modelirana s $K(S) \cdot P$.

- Broj ubijenih stanica u jedinici vremena ovisi o ukupnom broju stanica.
- Povećanjem broja stanica očekujemo i povećanje broja ubijenih stanica
- $K(S) \cdot P$ je najjednostavnija funkcija koja to opisuje (parsimonija!)

Chemostat model:

$$P' = K(S)P - \omega P$$

$$S' = -K(S)\frac{P}{Y} + \omega(S - S_0)$$

Rast populacije ne ovisi o koncentraciji lijeka (S):

$$\implies K(S)P \rightarrow kP$$

Nema otjecanja stanica:

$$\implies \omega P \rightarrow 0$$

Model infuzije lijeka:

$$P' = kP - K(S)P$$

$$S' = -\alpha K(S)P + \omega(S - S_0)$$

Kako definirati funkciju $K(S)$?

$$K(0) = 0 \text{ i } K(\infty) = \beta < \infty$$

$$\implies K(S) = \frac{\beta S}{a + S}.$$

Zadatak. Modificirajte model. Pretpostavku o eksponencijalnom rastu zamijenite logističkim ili Gompertzovim modelom.