Scaling Up for Modeling of Transport and Flow in Porous Media A conference in Honor of Alain Bourgeat

> A Fully Equivalent Global Pressure Formulation for Three-Phases Compressible Flows .

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Summary

- The three-phases immiscible compressible equations
- Why a global pressure ?
- Equivalent global pressure reformulation: TD Condition.
- An example of Global Capillary Pressure function
- TD-interpolation of two-phase data: compatibility condition
- Conclusions

Notations (1 = water, 2 = oil, 3 = gas)

• dependant variables :

$$\begin{cases} S_j = S_j(x,t) = reduced \ saturation, \ 0 \le S_j \le 1, \\ P_j = P_j(x,t) = pressure, \\ \varphi_j = \varphi_j(x,t) = volumetric \ flow \ vector \ at \ reference \ pressure \end{cases}$$

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• fluids and rock data :

$$\begin{cases} B_j = B_j(p_j) = \rho_j/\rho_j^{\text{ref}} = volume \ factor, \\ d_j = d_j(p_j) = B_j/\mu_j = phase \ mobility, \\ \phi = \phi(x, P_{pore}) = porosity, \\ K = K(x) = absolute \ permeability, \\ kr_j = kr_j(s_1, s_3) = phase \ relative \ permeability, \\ g = gravity \ constant, \\ Z = Z(x) = depth. \end{cases}$$

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Three Phases Equations

• conservation laws :

$$\frac{\partial}{\partial t} \{ \phi B_j(P_j) S_j \} + \nabla \cdot \varphi_j = 0 \quad , \quad j = 1, 2, 3.$$

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Three-phase equations - p. 4/19

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• capillary pressure law :

$$\begin{cases} P_1 - P_2 = P_c^{12}(S_1) , \\ P_3 - P_2 = P_c^{32}(S_3) , \end{cases}$$

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Three-phase equations - p. 4/19

An example of three-phase relative permeabilities



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Three-phase equations - p. 5/19

An example of capillary pressures



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Three-phase equations – p. 6/19

Classical resolution : "pressure" equation

$$\frac{\partial}{\partial t} \left\{ \phi \sum_{j=1}^{3} B_j S_j \right\} + \nabla \cdot q = 0 ,$$

where q is the global volumetric flow vector:

$$q = \sum_{j=1}^{3} \varphi_j = -K\lambda \{ \nabla P_2 + f_1 \nabla P_c^{12} + f_3 \nabla P_c^{13} - \rho g \nabla Z \}$$

$$\begin{cases} \lambda(s_1, s_3, p_2) &= \sum_{j=1}^3 kr_j d_j = global \ mobility, \\ f_j(s_1, s_3, p_2) &= kr_j d_j / \lambda = j^{th} \ fractional \ flow, \ \sum_{j=1}^3 f_j = 1, \\ \rho(s_1, s_3, p_2) &= \sum_{j=1}^3 f_j \rho_j = global \ density. \end{cases}$$

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classical resolution - p. 7/19

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Solve for the oil pressure P_2 ?

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classical resolution - p. 7/19

Behaviour of individual phase pressures

Case of a two-phase water-oil flow : oil and water pressures are singular near front boundary





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Let us have a dream... oil pressure



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Let us have a dream... - p. 9/19

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and P governs the global volumetric flow vector q:

$$q = -Kd\{\nabla P - \rho g \nabla Z\} \quad ?$$

(where $d(s_1, s_3, p) = \lambda(s_1, s_3, p_2)$)

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Let us have a dream... - p. 9/19

• how to replace : $q = -K\lambda\{\nabla P_2 + f_1\nabla P_c^{12} + f_3\nabla P_c^{13} - \rho g\nabla Z\}$ by : $q = -Kd\{\nabla P - \rho g\nabla Z\}$?

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for all
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and $s = (s_1, s_3) \in \mathbb{T}$.

The Global Capillary Pressure function $P_{ca-p.11/19}$

water

gas

S

 \mathbb{T}

 S_3

 s_1

oil

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- A natural parametrization of TD-three-phase data is made of :
- a global capillary function : $s \in \mathbb{T}, P_{\min} \leq p \leq P_{\max} \rightsquigarrow P_{cg}(s, p)$ satisfying : $\partial P_{cg} / \partial P(s, p) \leq k < 1$,
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- a global mobility function : $s \in \mathbb{T}, P_{\min} \leq p \leq P_{\max} \rightsquigarrow d(s, p)$.
- the associated fractional flows and relative permeabilities are :

 $\nu_{j}(s,p) = \partial P_{cg}/\partial s_{j}(s,p) / dP_{c}^{j2}/ds_{j}(s_{j}) , \quad j = 1,3$ $\begin{cases} kr_{j}(s,p) = \nu_{j}(s,p)d(s,p)/d_{j}(p - P_{cg}(s,p) + P_{c}^{j2}(s_{j})) & j = 1,3, \\ kr_{2}(s,p) = (1 - \nu_{1}(s,p) - \nu_{3}(s,p))d(s,p)/d_{2}(p - P_{cg}(s,p)), \end{cases}$

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Conclusion for the global pressure formulation -p. 12/19

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• by construction, TD-three-phase data satisfy :

$$\frac{\partial \nu_1}{\partial S_3}(s, \mathbf{p}) \frac{dP_c^{12}}{dS_1}(s_1) = \frac{\partial \nu_3}{\partial S_1}(s, \mathbf{p}) \frac{dP_c^{32}}{dS_3}(s_3) ,$$

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Conclusion for the global pressure formulation -p. 12/19

An example of global capillary pressure function



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An example of global capillary pressure – p. 13/19



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An example of global capillary pressure – p. 14/19

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$$s \in \mathbb{T} \rightsquigarrow \textbf{P_{cg}}(s,p) \ , \ s \in \mathbb{T} \rightsquigarrow \textbf{d}(s,p)$$



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ta - 1 gas the first of the second se

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produce relative permeabilities :

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which coincide with the given two-phase data on $\partial \mathbb{T}$.

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water - oil data

oil

gas

water

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 $\begin{array}{l} \text{if the fractional flows} \\ f_1(s,p_2) \ , \ f_3(s,p_2) \\ \text{are known along a curve} \\ \psi \\ \text{then P_{cg}} \ , \ \frac{\partial P_{cg}}{\partial S_1}(s,p) \ , \ \frac{\partial P_{cg}}{\partial S_3}(s,p) \\ \text{are known along the same curve.} \end{array}$



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TD-interpolation of two-phase data - 2 - p. 16/19

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TD-interpolation of two-phase data - 3 - p. 17/19

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- on the water-gas side $\implies P_{cg}^{\text{data}}$
- on the water-oil-gas sides $\implies P_{cq}^{\mathrm{data}}$



Let p = given global pressure level.

- Determination of P_{cg}^{data} on $\partial \mathbb{T}$: solve the differential equation
- on the water-gas side $\implies P_{cg}^{\text{data}}$
- on the water-oil-gas sides $\implies P_{cq}^{\mathrm{data}}$
- TD-compatibility condition :

 $P_{cg}^{\text{data}}(\text{gas}) = P_{cg}^{\text{data}}(\text{gas})$ or, in term of fractional flows at global pressure p :



$$\int_0^1 (\nu_1^{12,\text{data}} - \nu_1^{13,\text{data}}) \frac{dP_c^{12}}{ds_1} + \int_0^1 (\nu_3^{32,\text{data}} - \nu_3^{31,\text{data}}) \frac{dP_c^{32}}{ds_3} = 0$$

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• Determination of $(\partial P_{cg}/\partial n)^{\mathrm{data}}$ on $\partial \mathbb{T}$: use u_1 and u_3 .

Dubrovnik, October 13-16 2008

TD-interpolation of two-phase data - 3 - p. 17/19

• Determination of d^{data} on $\partial \mathbb{T}$ at global pressure p :

$$d^{\text{data}} = \begin{cases} kr_1^{12} d_1(p - P_{cg}^{\text{data}} + P_c^{12}) + kr_2^{12} d_2(p - P_{cg}^{\text{data}}) & \text{(water-oil)} \\ kr_1^{13} d_1(p - P_{cg}^{\text{data}} + P_c^{12}) + kr_3^{13} d_3(p - P_{cg}^{\text{data}} + P_c^{32}) \text{(gas-water)} \\ kr_3^{32} d_3(p - P_{cg}^{\text{data}} + P_c^{32}) + kr_2^{32} d_2(p - P_{cg}^{\text{data}}) & \text{(gas-oil)} \end{cases}$$

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• Possible choices for P_{cg} and d on \mathbb{T} at global pressure p:

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- by smooth interpolation :

$$\begin{cases} \Delta^2 P_{cg} = 0 & \text{in } \mathbb{T} ,\\ P_{cg} = P_{cg}^{\text{data}} & \text{on } \partial \mathbb{T} ,\\ \frac{\partial P_{cg}}{\partial n} = \frac{\partial P_{cg}^{\text{data}}}{\partial n} & \text{on } \partial \mathbb{T} , \end{cases} \begin{cases} -\Delta d = 0 & \text{in } \mathbb{T} ,\\ d = d^{\text{data}} & \text{on } \partial \mathbb{T} . \end{cases}$$

Dubrovnik, October 13-16 2008

TD-interpolation of two-phase data - 4 - p. 18/19

• Determination of d^{data} on $\partial \mathbb{T}$ at global pressure p :

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- by optimization : use for example $kr_1^{\text{Stone}}(s)$, $kr_3^{\text{Stone}}(s)$ as targets.
 - Finite element parameterization : reduced HCT for P_{cg} , P^1 for d.

• Let the three sets of water-oil, gas-oil and water-gas two-phase data satisfy the TD-compatibility condition.

• Then they can be interpolated by TD-three-phase data by chosing, for each global pressure level *p* :

- a \mathcal{C}^1 global capillary pressure $P_{cg}:\mathbb{T} \rightsquigarrow \mathbb{R}$

- a \mathcal{C}^0 global mobility $d:\mathbb{T} \rightsquigarrow \mathbb{R}$

- in \mathbb{T} , P_{cg} and d can be chosen freely, for example :
 - by smooth interpolation : $\Delta^2 P_{cg} = 0$, $-\Delta d = 0$ in \mathbb{T} ,
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